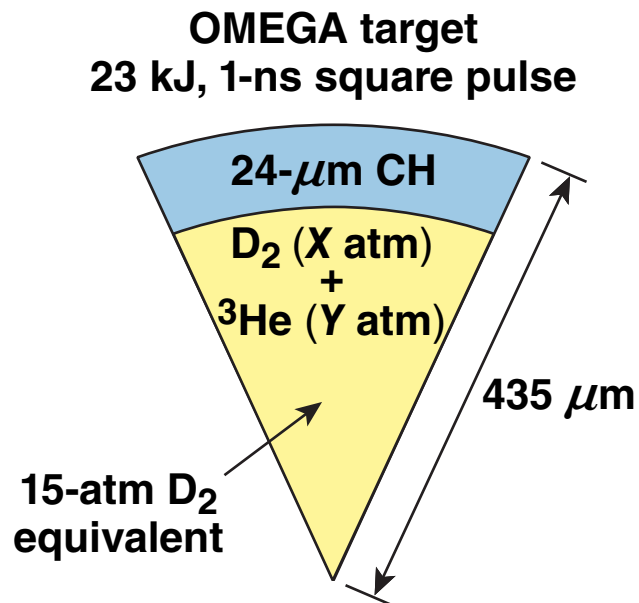
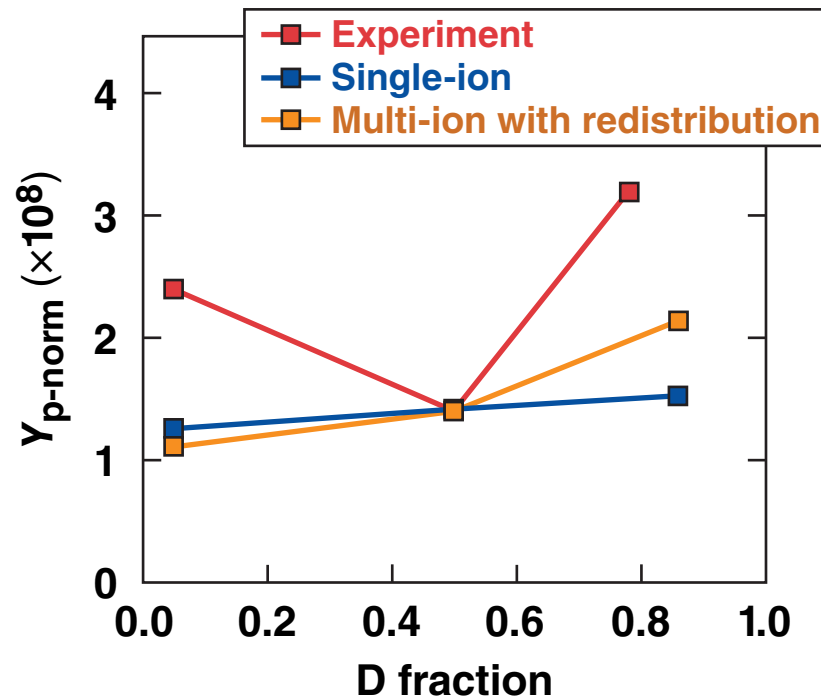


Modeling of Multiple-Ion Heat Transport in ICF Implosions



$$Y_{p\text{-norm}} = Y_p \frac{6 \text{ atm} \times 12 \text{ atm}}{X \times Y}$$



Multiple-ion effects in thermal conduction and mix were studied using the Chapman–Enskog method

- The dependence of neutron and proton yields in D^3He implosions on the D_2 fraction¹ cannot be explained with hydrosimulation using single-ion transport models.
- The multi-ion effects modify ion thermal conduction and lead to species diffusion due to gradients in hydro profiles.
- Results of the model indicate that the modification of ion conduction due to multiple-species effects is small.
- The diffusion mechanism produces trends consistent with the experimental data for D fraction larger than 50%.

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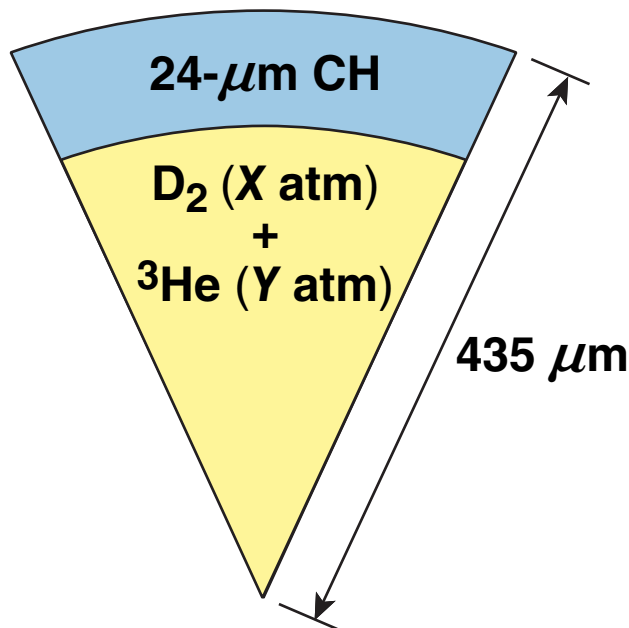
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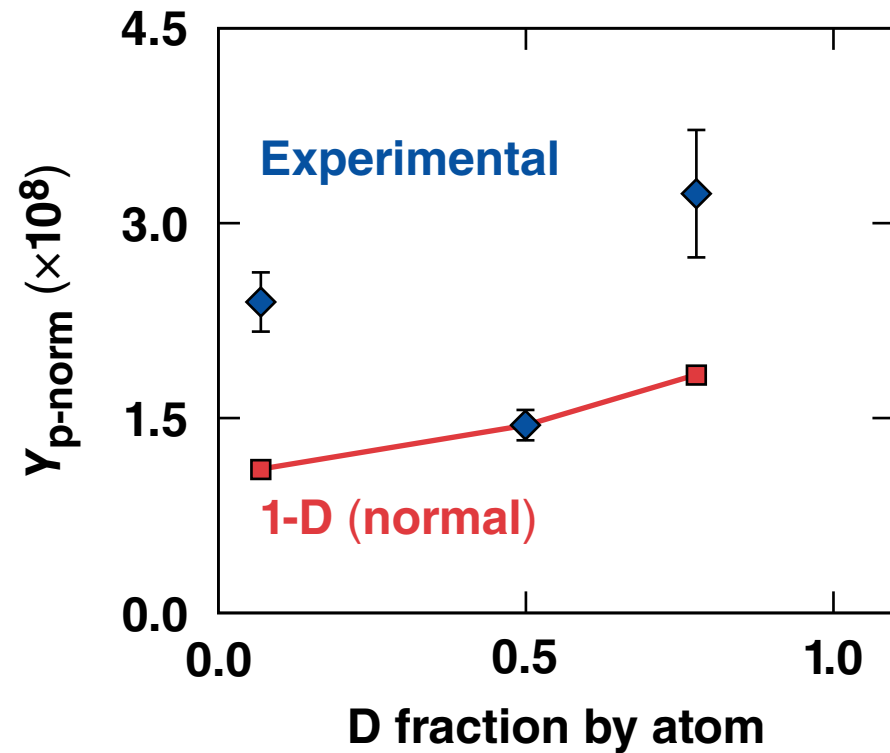
Motivation

The single-ion model deviates from the experiment measurement of neutron and proton yields

$$Y_p \propto X \times Y$$



$$Y_{p\text{-norm}} = Y_p \frac{6 \text{ atm} \times 12 \text{ atm}}{X \times Y}$$



The Chapman–Enskog method is used to derive transport coefficients

$$\frac{\partial f_1}{\partial t} + \vec{v} \frac{\partial f_1}{\partial \vec{r}} + \frac{e\vec{E}_1}{m_1} \frac{\partial f_1}{\partial \vec{v}} = J_{11} + J_{12} + J_{1e} \quad f_1 = f_M^1 + \delta f_1$$

$$(\mathbf{v} - \mathbf{u})_i \left(\mathbf{x} - \frac{5}{2} \right) \frac{\partial(\ln T)}{\partial r_i} + (\mathbf{v} - \mathbf{u})_i d_i + \frac{m_1}{T} V_{ij} \frac{\partial u_j}{\partial r_j} = \frac{J_{11} + J_{12}}{f_1}$$

Ion heat flux

Ion viscosity

$$d_i = \frac{\partial(\ln P_1)}{\partial r_i} - \frac{m_1}{\rho T} \frac{\partial P_T}{\partial r_i} + \frac{1}{P_1} \frac{\partial P_e}{\partial r_i} \frac{n_1 Z_1^2}{n_1 Z_1^2 + n_2 Z_2^2} + \frac{n_2 Z_1 Z_2 (Z_1 - Z_2) e E_i}{T(n_1 Z_1^2 + n_2 Z_2^2)}$$

The Chapman–Enskog method is used to derive transport coefficients

$$\frac{\partial f_1}{\partial t} + \vec{v} \frac{\partial f_1}{\partial \vec{r}} + \frac{e\vec{E}_1}{m_1} \frac{\partial f_1}{\partial \vec{v}} = J_{11} + J_{12} + J_{1e} \quad f_1 = f_M^1 + \delta f_1$$

$$x = \frac{m_1(v-u)^2}{2T}$$

$$(v-u)_i \left(x - \frac{5}{2} \right) \frac{\partial(\ln T)}{\partial r_i} + (v-u)_i d_i + \frac{m_1}{T} V_{ij} \frac{\partial u_j}{\partial r_j} = \frac{J_{11} + J_{12}}{f_1}$$

$(v-u)_i (v-u)_j - \frac{1}{3} (v-u)^2 \delta_{ij}$
 \downarrow
 V_{ij}
Ion viscosity

\uparrow
 $\frac{\partial(\ln T)}{\partial r_i}$
Ion heat flux

$$d_i = \frac{\partial(\ln P_1)}{\partial r_i} - \frac{m_1}{\rho T} \frac{\partial P_T}{\partial r_i} + \frac{1}{P_1} \frac{\partial P_e}{\partial r_i} \frac{n_1 Z_1^2}{n_1 Z_1^2 + n_2 Z_2^2} + \frac{n_2 Z_1 Z_2 (Z_1 - Z_2) e E_i}{T(n_1 Z_1^2 + n_2 Z_2^2)}$$

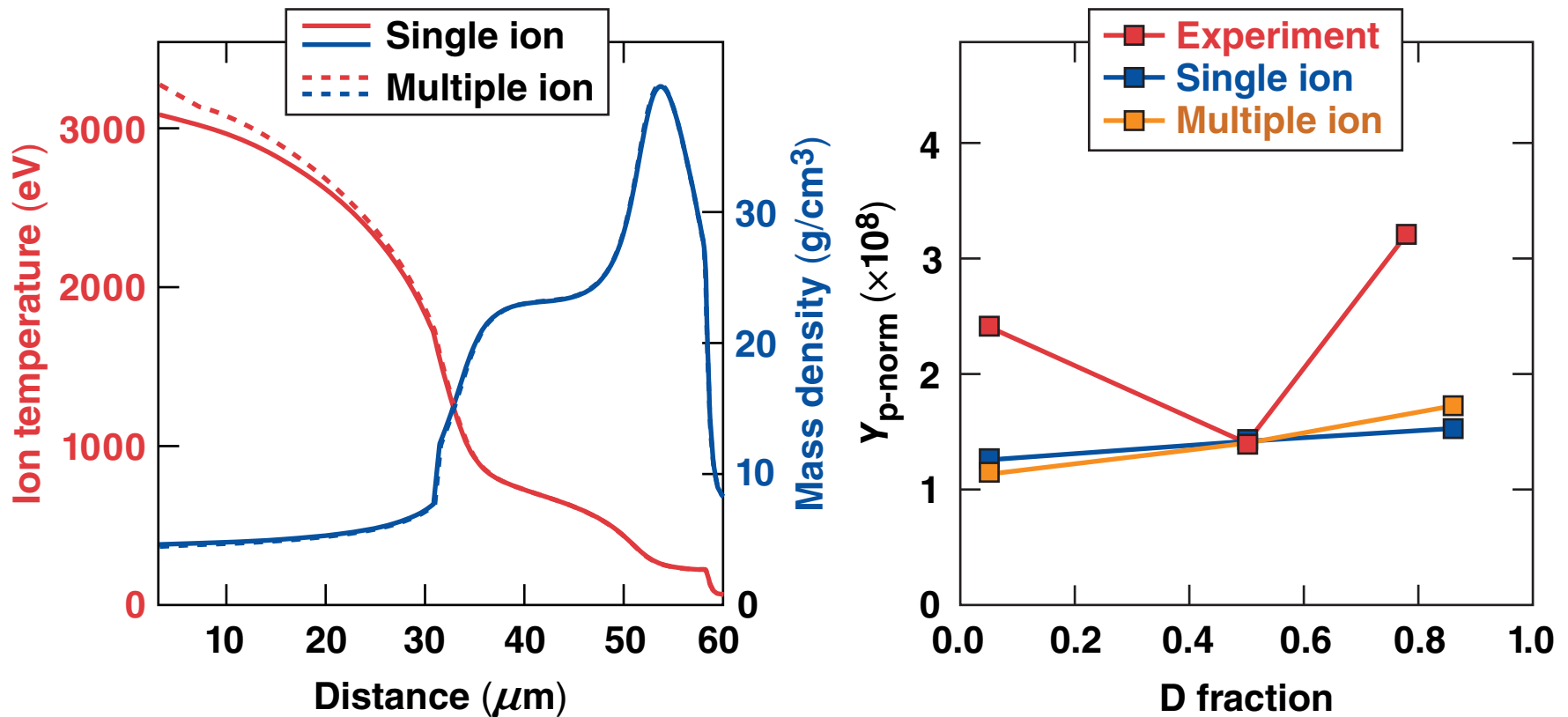
Ion heat flux and diffusion velocity depend on ion temperature and pressure gradient

$$\delta f_1 = f_M^1 (v - u)_i \left[\Phi_1(v) \frac{\partial \ln T}{\partial r_i} + \Phi_2(v) d_i \right]$$

$$\Phi(x) = \sum_n a_n L_n^{3/2}(x)$$

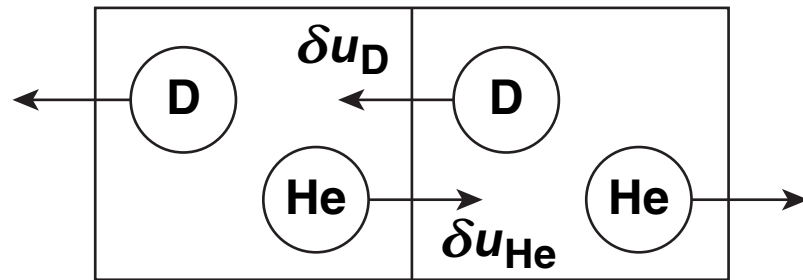
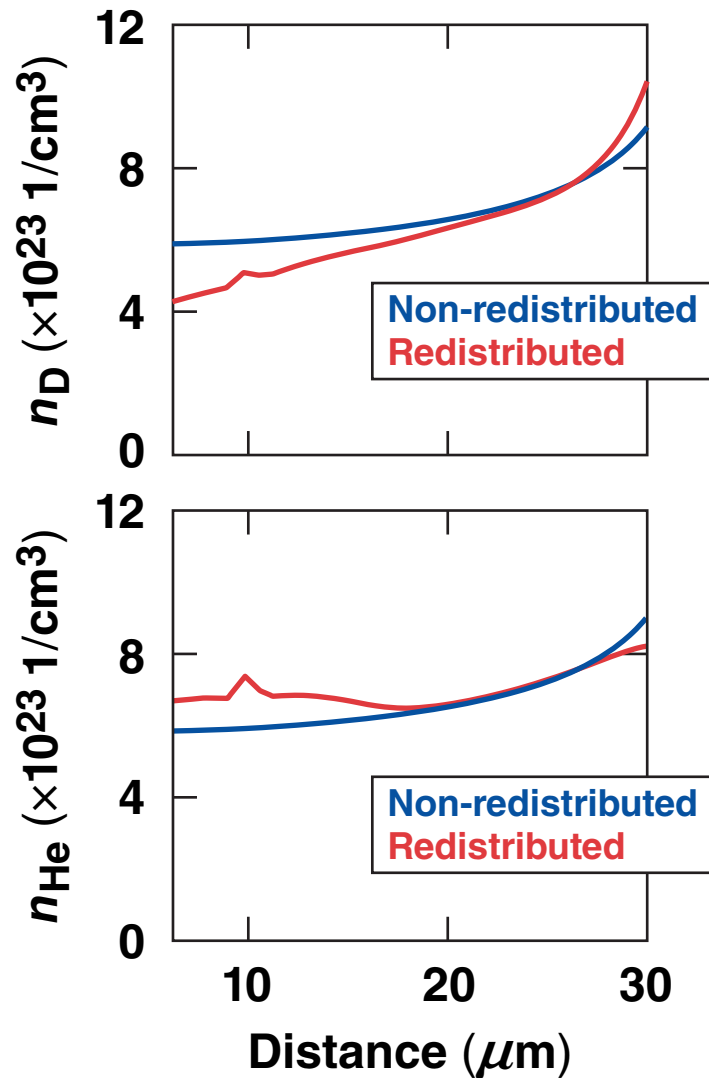
$$\vec{q}_1 = \int \vec{v} \frac{mv^2}{2} \delta f_1 d\vec{v} \quad \delta \vec{u}_1 = \frac{1}{n_1} \int \vec{v} \delta f_1 d\vec{v}$$

The modifications due to multi-ion conduction to the hydro profile are small



Only the modifications to the thermal conduction are included.

The difference in diffusion velocity leads to the particle redistribution

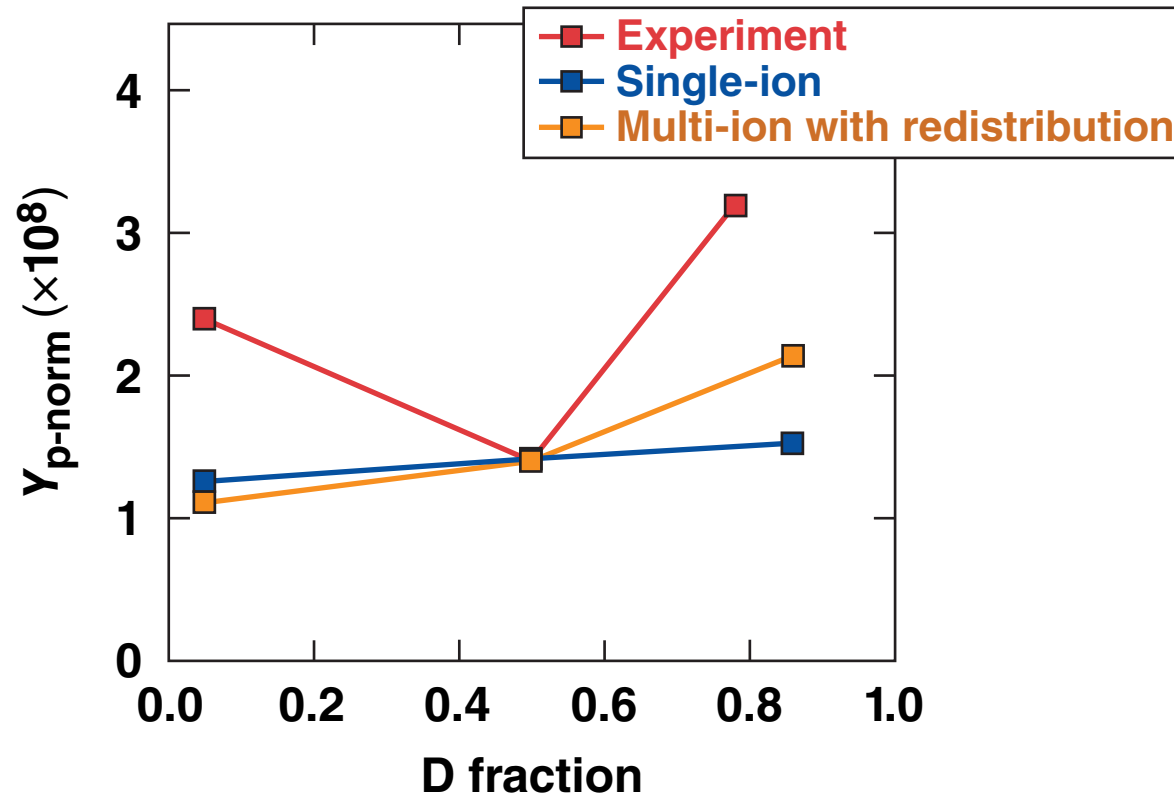


$$\delta u_D \neq \delta u_{\text{He}}$$

$$m_D n_D \delta u_D + m_{\text{He}} n_{\text{He}} \delta u_{\text{He}} = 0$$

Redistributed density is used only to calculate the reaction rate.

The trend predicted by the diffusion mechanism is consistent with the experiment for large D fraction



- $Q_{ie} \text{ (single-ion)} = \frac{3m_e}{\langle m_i \rangle} \frac{n_e}{\tau_{ei}} (T_e - T_i)$

- $Q_{ie} \text{ (multi-ion)} = 3m_e n_e (T_e - T_i) \left(\frac{1}{m_1 \tau_{e1}} + \frac{1}{m_2 \tau_{e2}} \right)$

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