

*Water Collection on a Platinum-Coated Molecular Sieve*

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## Abstract

Tritium is a radioactive isotope of hydrogen gas that is used regularly in experiments at the Laboratory for Laser Energetics (LLE). To prevent emissions to the environment, capture and containment of tritium released from process systems is very important. Air detritiation systems oxidize elemental tritium to form tritiated water (HTO), which is then collected on a molecular sieve drier. Tests were conducted to determine whether or not a platinum-coated molecular sieve (Pt/4A MS) loaded with light water (H<sub>2</sub>O) could serve as an alternative to the classical ‘burn and dry’ approach of capturing tritiated water currently employed (1). In these tests, deuterium was used as a surrogate for tritium. Deuterium gas in a helium carrier was converted to heavy water over a hot copper/zinc getter bed (2,3) and flowed over a platinum-coated 4A molecular sieve preloaded with light water. The dependence of the amount of heavy water captured in the molecular sieve on flow rate was measured.

### 1. Introduction

Currently, at LLE, the tritium removal from Omega and processes that contain tritiated air utilize the conventional “burn and dry” detritiation method (4). This comprises the conversion of elemental tritium to oxide using hot copper oxide, Hopcalite, or a precious metal catalyst (Pd, Pt), a molecular sieve drier and a tritium monitor. Although this system serves its purpose, conversion of HT to water over Hopcalite requires the presence of oxygen. A novel method of detritiation, explored in these experiments, may offer a simpler and more versatile solution. A platinized molecular sieve (Pt/4A MS) preloaded with light water (H<sub>2</sub>O) may eliminate the need for an oxidizer and drier. These two options are illustrated in Figure 1. In cases where the water content in the air stream is high, a condenser can be installed in front of the drier to extend the operational lifetime of the drier as shown in Figure 1.

In this experiment, a Pt/4A MS was tested for its ability to remove tritiated water ( $T_2O$ ) from an air stream with high humidity. The purpose of this experiment was to determine whether or not a Pt/4A MS, preloaded with  $H_2O$ , could adsorb a significant amount of  $T_2O$ , using  $D_2O$  as a surrogate. The efficiency and capacity at different flow rates of deuterium were also tested in the experiments.

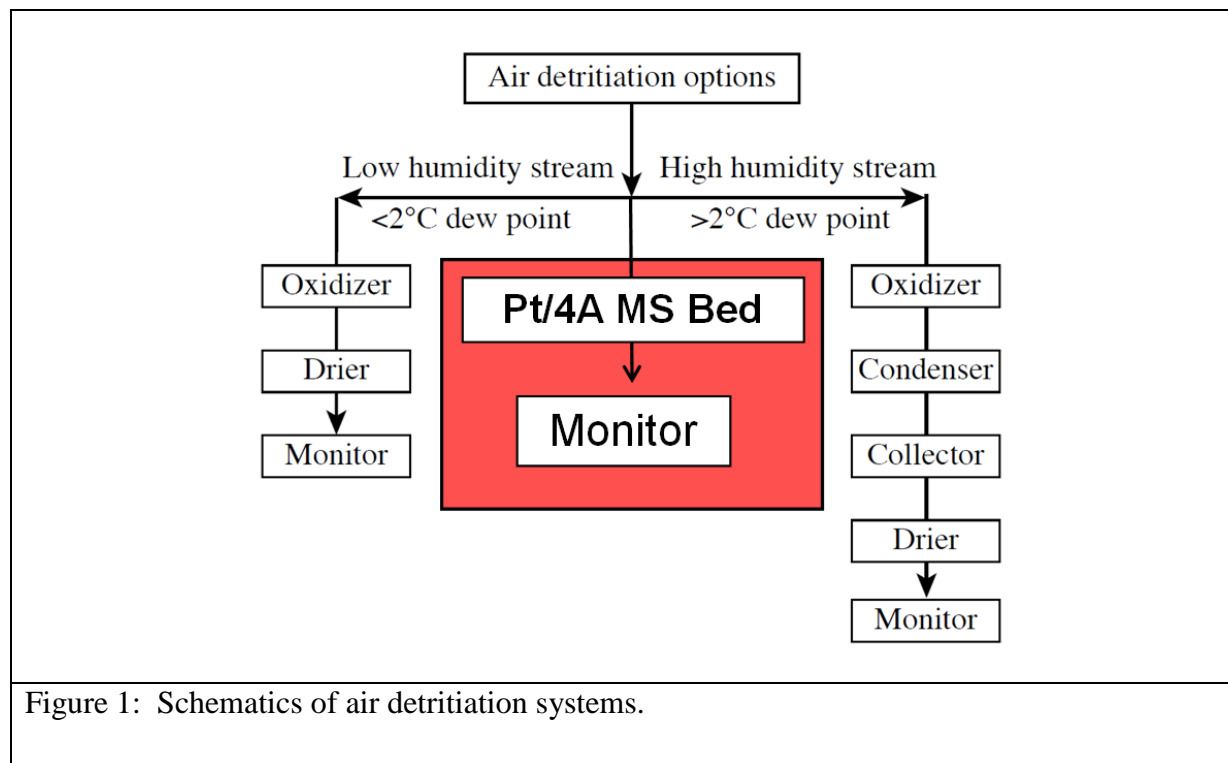


Figure 1: Schematics of air detritiation systems.

## 2. Experimental

### 2.1. System Configuration

A system was built to test how much  $D_2O$  could be loaded on to a Pt/4A MS, preloaded with  $H_2O$ . The system is organized into three sections:  $D_2O$  production, isotopic exchange, and hydrogen/deuterium detection. As seen in Figure 2, there are four gas cylinders containing He, 1%  $O_2$  in He,  $D_2$ , and compressed air. The gases, whose flow rates are controlled by mass flow controllers (MFC), are flowed either through a bed or through a bypass. The gases are monitored

downstream of both beds by the atmospheric sampling system, including a diaphragm pump, a turbomolecular pump, and a residual gas analyzer (RGA). An RGA measures the partial pressures of gases in the system. The nitrogen partial pressure was measured to ensure that no air leaked into the system during loading of the Cu/Zn getter bed. The total pressure could also be measured. A dew point sensor measured the humidity of the compressed air being flowed into the system. Thermocouples were used to control the temperatures of the Cu/Zn getter bed, the Pt/4A MS bed, and the heating tape used around the capillary tubing as well as select areas of piping. Capillary tubing connects the system with the RGA/ Atmospheric Sampling System and allows sampling during the experiments.

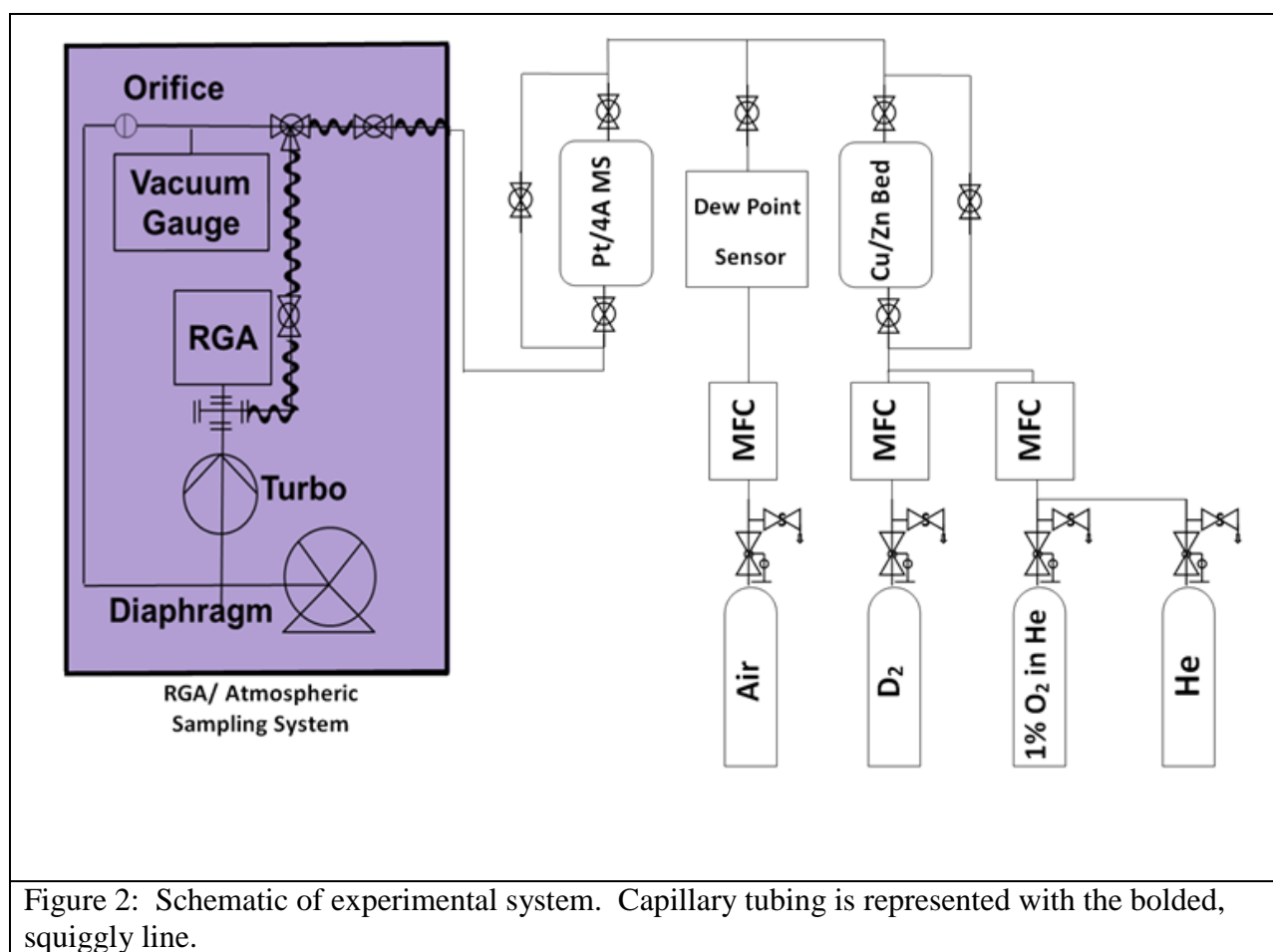
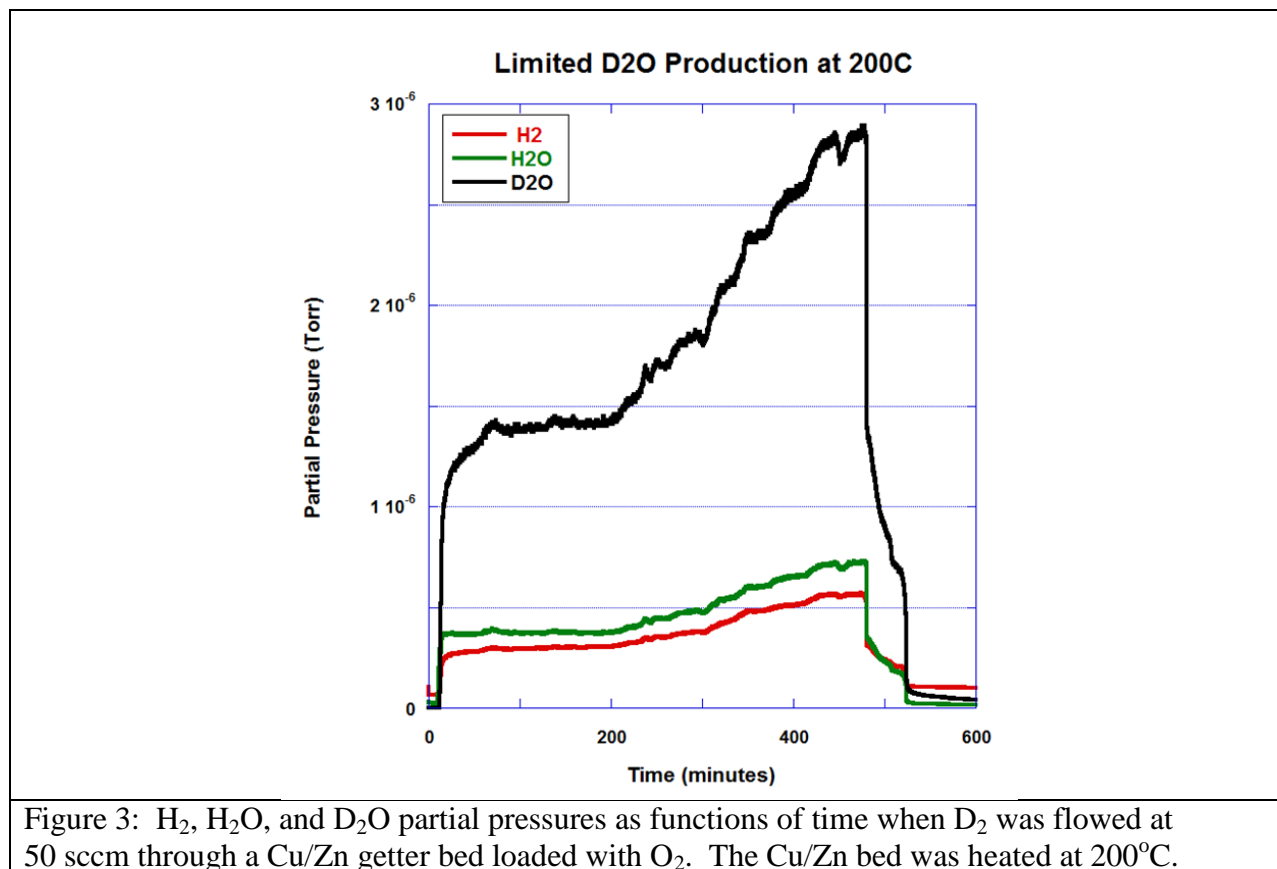


Figure 2: Schematic of experimental system. Capillary tubing is represented with the bolded, squiggly line.

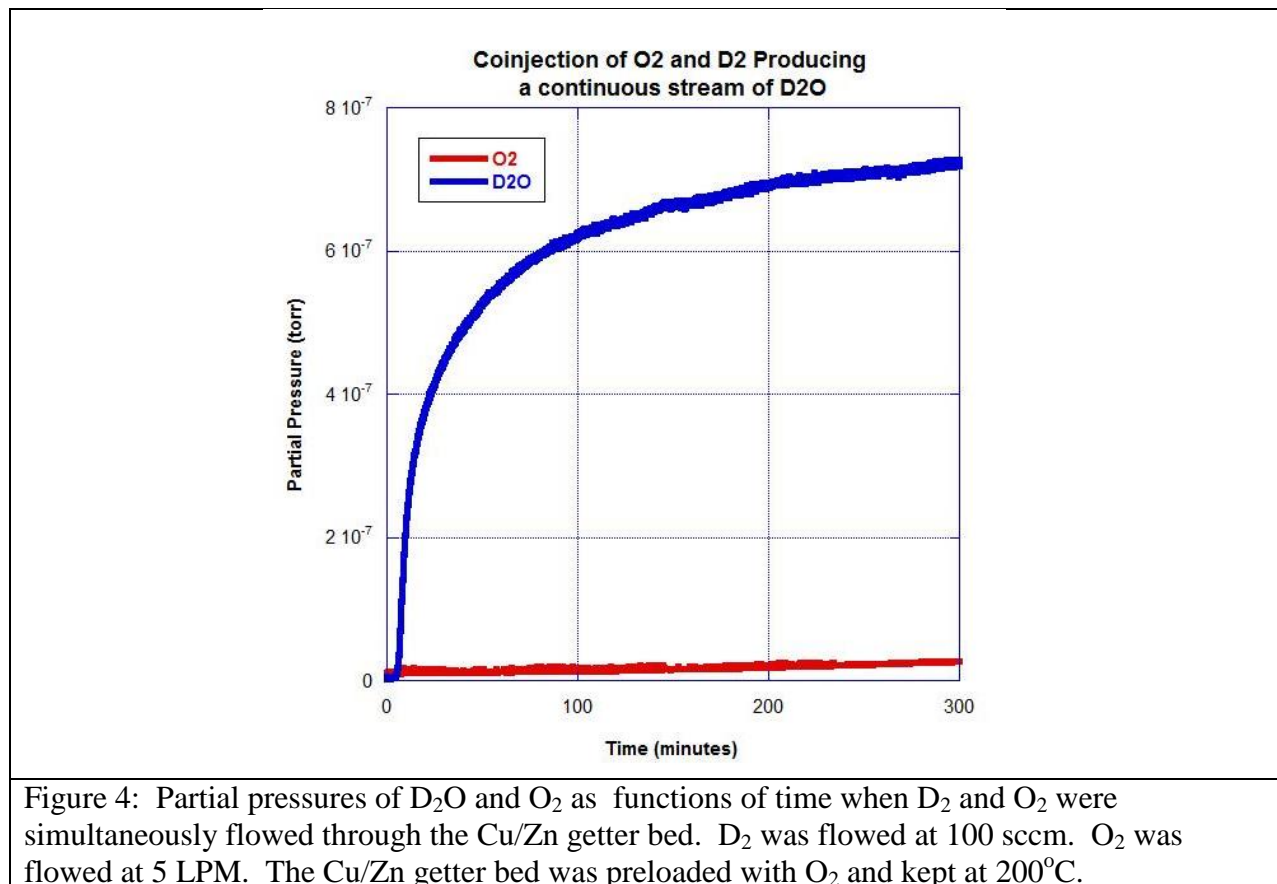
## 2.2. Experimental Procedure:

### 2.2.1 Formation of D<sub>2</sub>O:

The Cu/Zn getter bed was heated to 200°C, and 1% O<sub>2</sub> in He was flowed at 5 LPM (liters per minute) through the bed. The Pt/4A MS bed was bypassed such that no oxygen flowed through it. Once filled to capacity, the getter bed was bypassed, and He was flowed at 5 LPM to purge the system. Once the system was purged, the Cu/Zn getter bed was re-opened and D<sub>2</sub> was flowed through it at 50 sccm (standard cubic centimeters per minute). As seen in Figure 3, a stream of D<sub>2</sub>O was produced for approximately 500 minutes before D<sub>2</sub>O production began to decrease. This occurred when the oxidized Cu/Zn was reduced to elemental Cu/Zn and no more O<sub>2</sub> was available. Because the stream of D<sub>2</sub>O was not continuous over a long period of time, this method of D<sub>2</sub>O production was referred to as the “limited production method”.



It was found that this method of D<sub>2</sub>O production would not suffice for full runs, a full run meaning an experiment where D<sub>2</sub>O is flowed through a Pt/4A MS bed preloaded with H<sub>2</sub>O until complete D<sub>2</sub>O breakthrough occurs from the Pt/4A MS bed without running out of D<sub>2</sub>O on the Cu/Zn bed. Instead, it was determined that a constant stream of D<sub>2</sub>O would be necessary. To produce a constant, unlimited flow of D<sub>2</sub>O, D<sub>2</sub> and 1% O<sub>2</sub> in He were co-injected into the system through the Cu/Zn getter bed, which was preloaded to capacity with O<sub>2</sub>. D<sub>2</sub> was flowed at 100 sccm and 1% O<sub>2</sub> was flowed at 5 LPM. This method, referred to as the “continuous production method,” proved to be successful. As seen in Figure 4, a stable D<sub>2</sub>O stream leaving the bed approaches a steady state level after approximately 300 minutes.



### **2.2.2 Loading Pt/4A MS with H<sub>2</sub>O:**

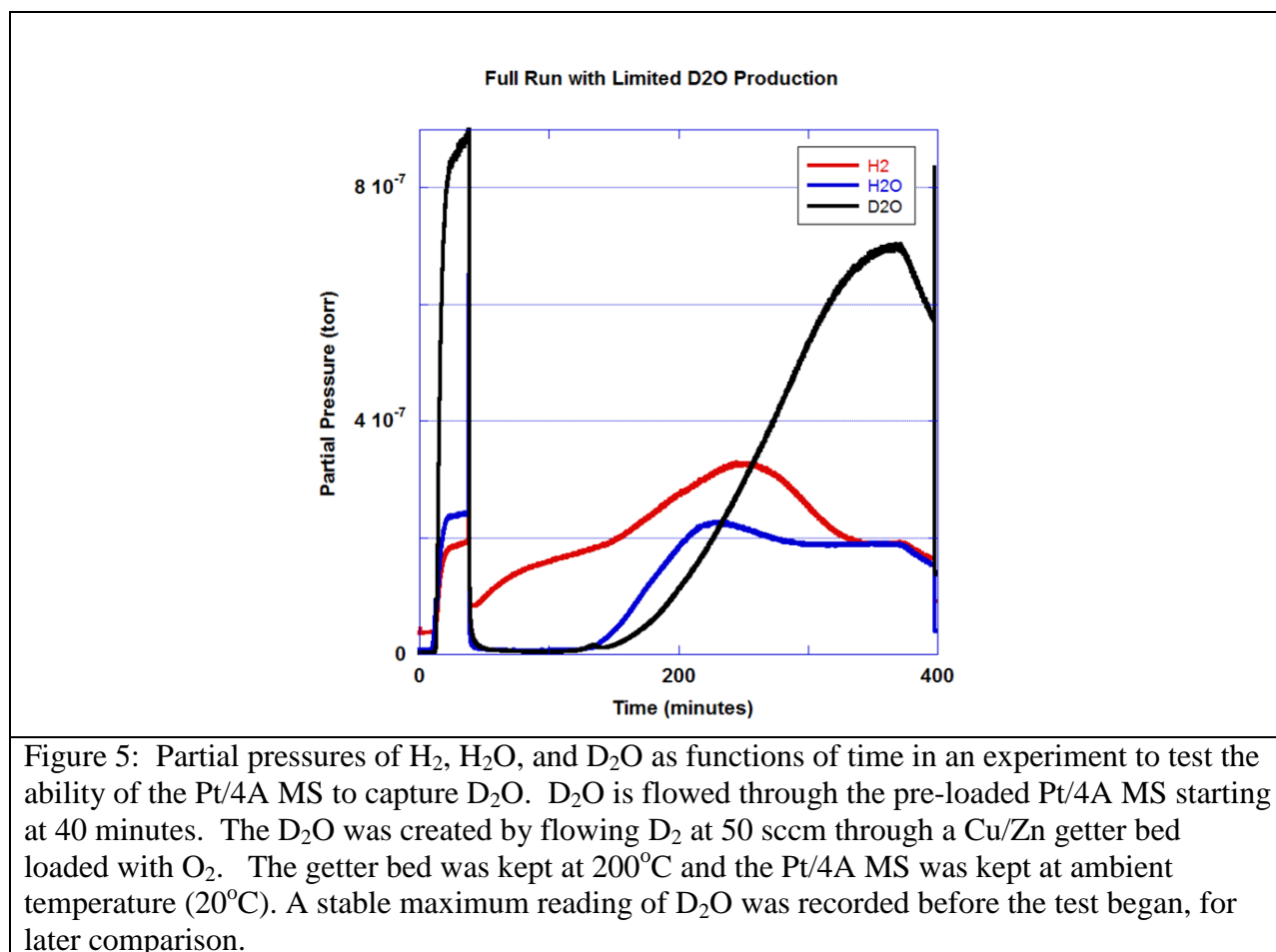
To prepare the Pt/4A MS for operation in humid air streams, the Pt/4A MS bed was pre-loaded with H<sub>2</sub>O. This medium was chosen because of its ability to capture H<sub>2</sub>O. The interatomic space between the neighbor cages of the molecular sieve is four-angstrom. Four angstrom molecular sieves have the ability to adsorb H<sub>2</sub>O without altering its chemical composition, allowing it to extract H<sub>2</sub>O from flowing gas streams. When loading the Pt/ 4A MS with H<sub>2</sub>O, the Cu/Zn getter bed was valved so as to isolate the Cu/Zn getter from the H<sub>2</sub>O. Initially, compressed air was flowed at 1 LPM, such that a 100% air flow pressure was recorded for later comparison. The air flow was turned off, and He was flowed at 1 LPM to purge the system. The Pt/4A MS bed was opened, still only flowing He at 1 LPM. Once air levels were back down to background levels, the He flow was stopped and the air flow was turned on at 1 LPM.

### **2.2.3 Full Experiment:**

Once the system was set up for a full experiment (i.e. the Cu/Zn bed was loaded to capacity with O<sub>2</sub> and the Pt/4A MS was loaded with H<sub>2</sub>O), co-injection of D<sub>2</sub> and 1% O<sub>2</sub> in He began through the Cu/Zn getter bed which was preheated to 200°C . Once a stable maximum reading of D<sub>2</sub>O production was recorded, the Pt/4A MS bed was opened and its bypass closed. Full runs were performed at three different flow rates of D<sub>2</sub>. After a full run was completed, the system was purged and reset. To purge the system, the Pt/4A MS was heated to 150°C, and He was flowed through it at 2 LPM. After 120 minutes, the temperature of the Pt/4A MS was increased to 200°C.

### 3. Results:

The results of one run using the limited production method are shown in Figure 5. The results show that D<sub>2</sub>O can, indeed, be stored on the loaded Pt/4A MS, and that the Pt/4A MS is capable of adsorbing significant amounts of D<sub>2</sub>O. The amount of D<sub>2</sub>O is comparable to the amount of H<sub>2</sub>O that can be stored. Prior to a full test, approximately 8g H<sub>2</sub>O /gMS was loaded onto the Pt/4A MS. When D<sub>2</sub>O was flowed through the pre-loaded Pt/4A MS using the limited production method, approximately 5g of additional D<sub>2</sub>O/g MS was loaded onto the Pt/4A MS.





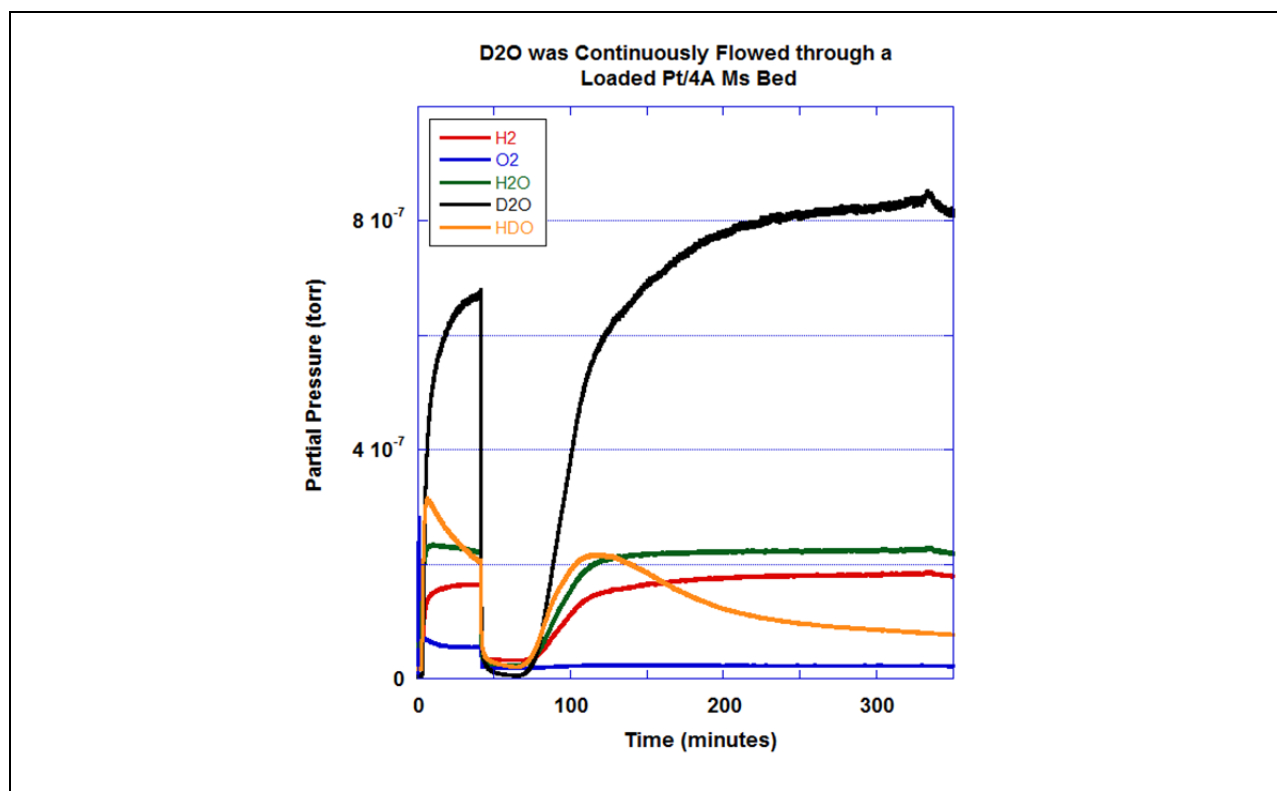


Figure 6: Partial pressures of H<sub>2</sub>, O<sub>2</sub>, H<sub>2</sub>O, D<sub>2</sub>O, and HDO as a function of time for an experiment similar to that of Figure 5 except that 1% O<sub>2</sub> in He was also flowed through the Cu/Zn getter bed. D<sub>2</sub> was flowed at 100 sccm. O<sub>2</sub> was flowed at 5 LPM. At 40 minutes, the Pt/4A MS was opened and D<sub>2</sub>O was allowed to flow through the Pt/4A MS.

High capture efficiencies were realized at superficial flow rates up to  $11 \text{ scc}/\text{min}/\text{cm}^2$ . In Figure 6, D<sub>2</sub> was co-injected with 1% O<sub>2</sub> in He at the respective rates of 100 sccm and 5 LPM. For 27 minutes, no D<sub>2</sub>O was recorded in the outlet stream, indicating that all D<sub>2</sub>O being produced was being absorbed by the Pt/4A MS. 27 minutes into the experiment, however, breakthrough occurred. Breakthrough refers to the time at which the concentration of D<sub>2</sub>O in the outlet stream reaches 1% of the value when the bed is bypassed, or, in this case,  $2.31 \times 10^{-9}$  torr. For the remainder of the experiment, the Pt/4A MS's ability to absorb D<sub>2</sub>O decreased until the maximum reading in the outlet stream was reached.

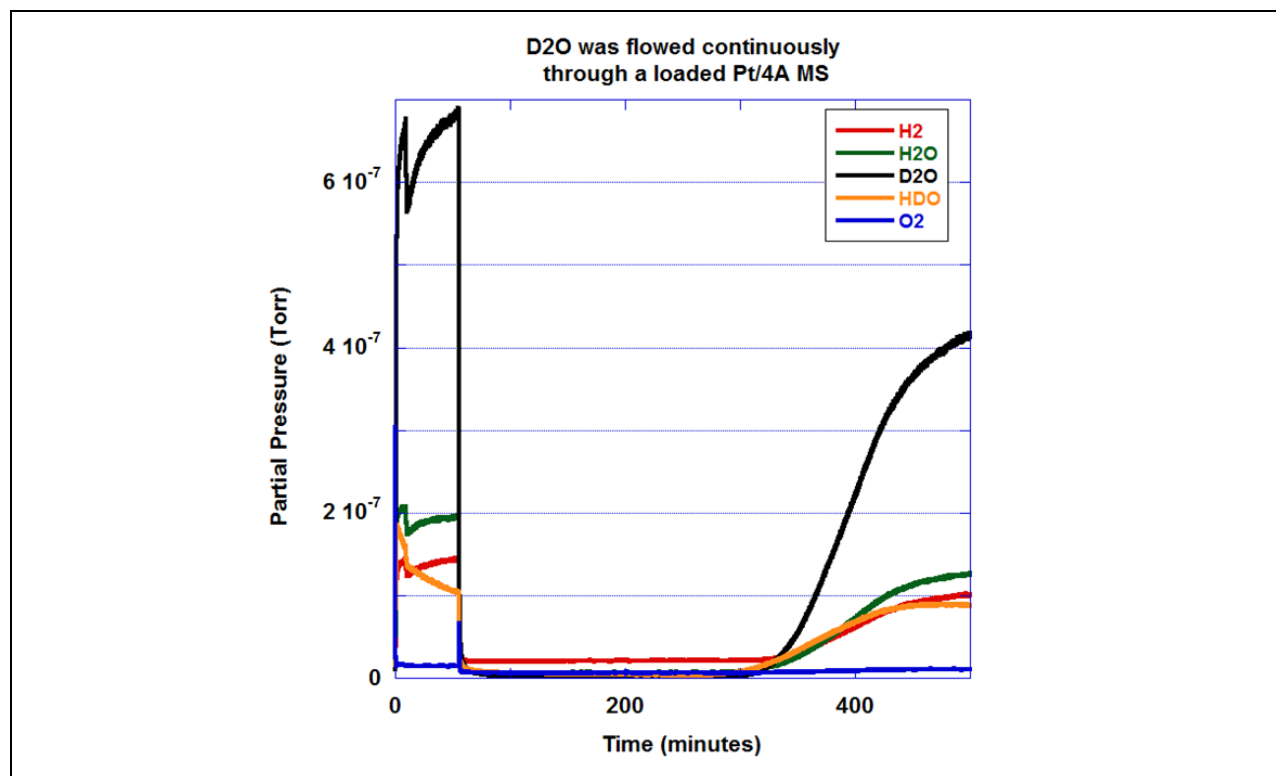


Figure 7: Partial pressures of H<sub>2</sub>, O<sub>2</sub>, H<sub>2</sub>O, D<sub>2</sub>O, and HDO as a function of time for an experiment similar to that of Figure 6 but with lower D<sub>2</sub> and O<sub>2</sub> flow rates. D<sub>2</sub> was flowed at 20 sccm. O<sub>2</sub> was flowed at 1 LPM. At 40 minutes, the Pt/4A MS was opened and D<sub>2</sub>O was allowed to flow through.

As shown in Figure 7, the same experiment was performed with D<sub>2</sub> flowing at a lower rate of 20 sccm, and 1% O<sub>2</sub> in He flowing at a rate of 1 LPM. In this experiment, breakthrough occurred 260 minutes into the experiment. The mass of D<sub>2</sub>O loaded onto the Pt/4A MS is shown in Table 1. Reducing the D<sub>2</sub>O residence time in the Pt/4A MS by a factor of 5 increases the storage capacity approximately two fold, even though the Pt/4A MS has been preloaded with H<sub>2</sub>O to capacity.

Flow Rate of D <sub>2</sub> O (sccm)	Mass of D <sub>2</sub> O Loaded onto Pt/4A MS (gD <sub>2</sub> O/gMS)
20	2.4
100	4.7

Table 1: Total mass of D<sub>2</sub>O loaded onto Pt/4A MS for runs at both D<sub>2</sub>O flow rates of 20 sccm and 100 sccm.

## Conclusions

Experiments were performed to determine whether a Pt/4A MS could serve as a novel and alternative method to the conventional “burn and dry” method for tritium extraction from a humid air stream. Tests were completed by flowing D<sub>2</sub>O through a Pt/4A MS preloaded with H<sub>2</sub>O, to simulate the humid air stream. Superficial flow rates were realized up to 11 scc/min/cm<sup>2</sup>. Results indicate that the Pt/4A MS has the capability of capturing up to 4.7g/g MS of D<sub>2</sub>O on a bed preloaded to capacity with H<sub>2</sub>O. These tests suggest that a simpler, more versatile technique of tritium capture and recovery can be implemented at LLE by preferential extractions of HTO from humid airstreams.

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## References

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